

## To the Editor:

The purpose of this letter is to address some conclusions drawn in the article entitled "Population balance model for nucleation, growth, aggregation and breakage of hydrate particles in turbulent flow" by Balakin et al.<sup>1</sup> Four modification coefficients are used in this article,  $k_1$ ,  $k_2$ ,  $k_3$ , and  $k_4$  for their models. These four coefficients are used for the nucleation, growth, aggregation and breakage terms, respectively. Among the units of these four coefficients, two of them are unusual and rather meaningless units, that the unit for  $k_3$  is  $\text{J}^{0.18}$ , and the unit for  $k_4$  is  $\text{s}^{b-1}/\text{m}^3$ . It is obvious that these are the results of dimensional analysis. The coefficient  $k_3$  appears in Eq. 14, and this equation is based on van de Ven and Mason's work.<sup>2</sup> The coefficient  $k_4$  appears in Eq. 16, and this equation was original raised up by Spicer and Pratsinis.<sup>3</sup>

Van de Ven and Mason<sup>2</sup> suggested an expression of collision efficiency  $\alpha$  that  $\alpha = k[H/(36\pi\mu\gamma\bar{r}^3)]^b$ , and emphasized  $H/(36\pi\mu\gamma\bar{r}^3)$  is a dimensionless number. Here,  $H$  is the Hamaker constant and the value is unavailable in literature. While in Balakin et al.'s article,<sup>1</sup> the  $k_3 = k \cdot H^b$  coefficient. It is clear that  $k_3 = 36\pi\mu\gamma\bar{r}^3\alpha$ . From the context, the shear rate  $\gamma$ , and the mean radius  $\bar{r}$  are known and viscosity is not listed. Why the authors expanded the dimensionless number and created a new coefficient with such nonphysical meaning unit  $\text{J}^b$  ( $b = 0.189$  and  $0.19$ )?

Second, the power shown in Eq. 16 is a semiempirical number from the experimen-

tal data of particles with radius 0.5, 1 and  $2 \mu\text{m}$ .<sup>2</sup> While in Balakin et al.'s article,<sup>1</sup> the size of particle is much larger, that  $r$  covers the range from 0 to  $400 \mu\text{m}$ . Some references,<sup>4,5</sup> suggested that when the size of particle is larger than  $100\text{--}250 \mu\text{m}$ , the van der Waals force can be neglected and the momentum transfer plays the main role in such flow. Hence, the power law shown in Eq. 16 cannot be used for such big particles. Same as what they did, the dimensionless number  $H/(36\pi\mu\gamma\bar{r}^3)$  (or  $k_3$  in the article), and the exponential coefficient  $b$  could be obtained from the experimental results when the particles are not so huge. However, the number of experimental data is too few for such data fitting. There are only two groups of experimental result for the mean particle diameter  $d$ , less than  $100 \mu\text{m}$  in the experimental data shown in Figures 3, 4 and 6. Each of the group involves a point showing the mean dia.  $d = 0 \mu\text{m}$  at time  $t = 0 \text{ s}$ . Definitely, these points should be there because they are artificial initial condition, somehow.

Third, for the breakage term, Barthelmes et al.<sup>6</sup> induced a new expression of breakage function from Spicer and Pratsinis's work.<sup>3</sup> Thus, the coefficient  $k_4$  are nondimensionalized that  $g = k_4 \left(\frac{G}{k_b}\right)^b \bar{r}$ , in which  $k_b = 1/\text{s}$  is used to match the dimension of the shear rate. Perhaps this expression can make the coefficient with

a fixed unit and more physical meaning, but the values are kept as the same as those listed in the article.

## Literature Cited

1. Balakin BV, Hoffmann AC, Kosinski P. Population balance model for nucleation, growth, aggregation and breakage of hydrate particles in turbulent flow by Balakin. *AIChE J.* 2010;56:2052–2062.2.
2. van de Ven TGM, Mason SG. The micro-rheology of colloidal dispersions, VII: Orthokinetic doublet formation of spheres. *Colloid Polym Sci.* 1977;255:468–479.
3. Spicer PT, Pratsinis SE. Coagulation and fragmentation: universal steady-state particle-size distribution. *AIChE J.* 1996;42:1612–1620.
4. Midi GDR. On dense granular flows. *Eur Phys J E, Soft Matter.* 2004;14:341–365.
5. Zhu HP, Zhou ZY, Yang RY, Yu AB. Discrete particle simulation of particulate systems: Theoretical developments. *Chem Eng Sci.* 2007;62:3378–3396.
6. Barthelmes G, Pratsinis SE, Buggisch H. Particle size distributions and viscosity of suspensions undergoing shear-induced coagulation and fragmentation. *Chem Eng Sci.* 2003;58:2893–2902.

Jun Huang

Dept. of Energy and Process Engineering  
Faculty of Engineering Science and Technology  
Norwegian University of Science and Technology  
Trondheim, 7491, Norway  
E-mail: jun.huang@ntnu.no